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**Liquid compositions and (co)polymers, processes for
preparing them, and their use for preparing reactive
multisubstance mixtures**

5 The present invention relates to novel liquid
compositions and (co)polymers and also to novel
processes for preparing them. The present invention
further relates to the use of the novel liquid
compositions and (co)polymers for preparing novel
10 reactive multisubstance mixtures, especially coating
compositions, adhesives and sealing compounds.

Multisubstance mixtures known today, especially coating
compositions, such as clearcoat or topcoat materials,
15 primer-surfacers, primers or motor vehicle underbody
protection compositions, adhesives or sealing
compounds, are based on binders which must have a large
number of different properties in order that the
requisite coating, bonding or sealing properties can be
20 achieved. Such multisubstance mixtures, especially
coating systems, are known, for example, from the
German patents DE-A-44 07 415, DE-A-44 07 409 or
DE-A-43 10 414. The disadvantage of all of these
multisubstance mixtures is that the solids contents
25 cannot be raised ad infinitum. With these systems,
therefore, reducing the solvent emission is possible

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only within narrow limits.

To a certain extent, this situation may be remedied through the use of reactive diluents. The reactive diluent comprises a reactive diluter or solvent which, according to the definition of DIN 55945: 1996-09, becomes part of the binder during the film forming process, as a result of chemical reaction. The use of customary and known reactive diluents in coating systems, for example, may, however, be accompanied by problems, such as the incipient dissolution of other coats during application, or the lowering of the heat stability and light stability. Moreover, the addition of reactive diluents to the coating systems represents an additional process step, which in view of the process economy is fundamentally disadvantageous.

Furthermore, the addition of reactive diluents to the customary and known multisubstance mixtures is unable to remove the problem that, for the preparation of the binders, it is still necessary to use solvents, which then determine the overall solvent content of the reactive multisubstance mixtures. Although it is possible in some cases to prepare the binders by polymerization in bulk, i.e., without solvent, problems then arise during mixing with the other constituents of

the reactive multisubstance mixtures, so that, ultimately, it is again necessary to have recourse to solvents.

5 It is an object of the present invention to provide novel liquid compositions and also novel (co)polymers which no longer have the disadvantages of the prior art but which instead allow reactive multisubstance mixtures which are virtually solvent-free to be
10 prepared without additional process steps. It is a further object of the present invention to provide novel multisubstance mixtures, especially novel coating compositions, adhesives and sealing compounds, which are especially simple to prepare and use. Not least, it
15 is an object of the present invention to propose a new process for (co)polymerizing olefinically unsaturated compounds.

The invention accordingly provides the novel liquid
20 compositions and the novel (co)polymers, which are obtainable by (co)polymerizing olefinically unsaturated compounds in reactive diluents for thermally curable reactive multisubstance mixtures as reaction medium.

25 In the light of the prior art it was surprising and unforeseeable for the skilled worker that the object on

which the present invention is based could be achieved by means of the novel liquid compositions and the novel (co)polymers. In particular, there was no reason to expect that the preparation of reactive multisubstance mixtures would be considerably simplified by the novel liquid compositions and novel (co)polymers.

In the text below, the novel liquid compositions are referred to as "compositions of the invention" and the novel (co)polymers are referred to as "(co)polymers of the invention".

Similarly, the novel reactive multisubstance mixtures are referred to as "multisubstance mixtures of the invention".

The compositions and (co)polymers of the invention are obtainable by (co)polymerizing olefinically unsaturated compounds.

Suitable olefinically unsaturated compounds are all monomers with a functionality of one or more which are customary and known in the field of plastics. In accordance with the invention it is of advantage to use monofunctional monomers, in order to prevent unwanted crosslinking or gelling of the (co)polymers during the

preparation. In many cases, however, it may be of advantage to use monomers of higher functionality as well, in minor amounts.

5 Examples of suitable monomers for use in accordance with the invention are

10 A1) olefins such as ethylene, propylene, but-1-ene, pent-1-ene, hex-1-ene, cyclohexene, cyclopentene, norbornene, butadiene, isoprene, cyclopentadiene or dicyclopentadiene,

15 A2) esters of (meth)acrylic acid which are substantially free from acid groups and hydroxyl groups, such as

(meth)acrylic alkyl or cycloalkyl esters having up to 20 carbon atoms in the alkyl radical, especially methyl, ethyl, propyl, n-butyl, sec-butyl, tert-butyl, hexyl, ethylhexyl, stearyl and lauryl acrylate or methacrylate; or cycloaliphatic (meth)acrylic esters, especially cyclohexyl, isobornyl, dicyclopentadienyl, octahydro-4,7-methano-1H-indenemethanol or tert-butyl-cyclohexyl (meth)acrylate;

25

(meth)acrylic oxaalkyl esters or oxacycloalkyl esters such as ethyl triglycol (meth)acrylate and methoxyoligoglycol (meth)acrylate having a molecular weight Mn of preferably 550 or other ethoxylated and/or propoxylated, hydroxyl-free (meth)acrylic acid derivatives;

ethylene glycol, propylene glycol, diethylene glycol, dipropylene glycol, butylene glycol, pentane-1,5-diol, hexane-1,6-diol, octahydro-4,7-methano-1H-indenedimethanol or cyclohexane-1,2-, -1,3- or -1,4-diol di(meth)acrylate; or

trimethylolpropane di or tri(meth)acrylate or pentaerythritol di-, tri- or tetra(meth)acrylate;

A3) (meth)acrylamides such as (meth)acrylamide, N-methyl-, N,N-dimethyl-, N-ethyl-, N,N-diethyl-, N-propyl-, N,N-dipropyl-, N-butyl-, N,N-dibutyl-, N-cyclohexyl- or N,N-cyclohexylmethyl-(meth)acrylamide;

A4) monomers which carry per molecule at least one hydroxyl group and are substantially free from acid groups, such as

hydroxyalkyl esters of acrylic acid, methacrylic acid or another alpha,beta-ethylenically unsaturated carboxylic acid, which are derived from an alkylene glycol, which is esterified with the acid, or are obtainable by reacting the acid with an alkylene oxide, especially hydroxyalkyl esters of acrylic acid, methacrylic acid, ethacrylic acid, crotonic acid, maleic acid, fumaric acid or itaconic acid, in which the hydroxyalkyl group contains up to 20 carbon atoms, such as 2-hydroxyethyl, 2-hydroxypropyl, 3-hydroxypropyl, 3-hydroxybutyl, 4-hydroxybutyl, octahydro-4,7-methano-1H-indenedimethanol or methylpropanediol monoacrylate, monomethacrylate, monoethacrylate, monocrotonate, monomaleate, monofumarate or monoitaconate; or reaction products of cyclic esters, such as epsilon-caprolactone, and these hydroxyalkyl esters;

olefinically unsaturated alcohols such as allyl alcohol or polyols such as trimethylolpropane monoallyl or diallyl ether or pentaerythritol monoallyl, diallyl or triallyl ether;

A5) monomers which carry per molecule at least one acid group, preferably a carboxyl, sulfonic or

phosphonic acid group, especially acrylic acid, methacrylic acid, ethacrylic acid, crotonic acid, maleic acid, fumaric acid, itaconic acid, mono(meth)acryloyloxyethyl maleate, mono(meth)-
5 acryloyloxyethyl succinate or mono(meth)acryloyloxyethyl phthalate;

10 A6) monomers containing epoxide groups, such as the glycidyl ester of acrylic acid, methacrylic acid, ethacrylic acid, crotonic acid, maleic acid, fumaric acid or itaconic acid;

15 A7) vinylaromatic hydrocarbons, such as styrene, alpha-alkylstyrenes, especially alpha-methylstyrene, or vinyltoluene;

A8) nitriles such as acrylonitrile or methacrylonitrile;

20 A9) reaction products of the above-described monomers (A5) with the glycidyl ester of an alpha-branched monocarboxylic acid having from 5 to 18 carbon atoms per molecule, especially the reaction product of acrylic and/or methacrylic acid with
25 the glycidyl ester of Versatic acid;

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A10) vinyl compounds such as vinyl chloride, vinyl fluoride, vinylidene dichloride, vinylidene difluoride; N-vinylpyrrolidone; vinyl ethers such as ethyl vinyl ether, n-propyl vinyl ether, isopropyl vinyl ether, n-butyl vinyl ether, isobutyl vinyl ether or vinyl cyclohexyl ether; vinyl esters such as vinyl acetate, vinyl propionate, vinyl butyrate, vinyl pivalate or the vinyl ester of 2-methyl-2-ethylheptanoic acid, or vinyl esters of alpha-branched monocarboxylic acids having from 5 to 18 carbon atoms in the molecule, which are obtained by reacting formic acid or carbon monoxide and water in the presence of a liquid, strongly acidic catalyst with propylene trimer, propylene tetramer or diisobutylene or with olefins which are cracking products of paraffinic hydrocarbons such as mineral oil fractions and contain both branched or straight-chain acyclic and/or cycloaliphatic olefins;

25

A11) polysiloxane macromonomers which have a number-average molecular weight M_n of from 1 000 to 40 000, preferably from 2 000 to 20 000, with particular preference from 2 500 to 10 000, and in particular from 3 000 to 7 000, and which contain

on average 0.5 to 2.5, preferably from 0.5 to 1.5, ethylenically unsaturated double bonds per molecule, as are described in DE-A-38 07 571 on pages 5 to 7, in DE-A 37 06 095 in columns 3 to 7, in EP-B-0 358 153 on pages 3 to 6, in US-A 4,754,014 in columns 5 to 9, in DE-A 44 21 823 or in the international patent application WO 92/22615 on page 12 line 18 to page 18 line 10, or acryloxysilane-containing vinyl monomers, preparable by reacting hydroxy-functional silanes with epichlorohydrin and then reacting the reaction product with methacrylic acid and/or hydroxyalkyl esters of (meth)acrylic acid;

In accordance with the invention, accordingly, the monomers may be selected such that the (co)polymerization results in any desired polymers and copolymers, such as polyolefins, polystyrenes, polybutadienes, polyisoprenes, polyvinyl chlorides, polyacrylonitriles, polyvinyl acetates or polyacrylates, for instance.

In accordance with the invention, however, it is of advantage to select the monomers such that the (co)polymerization results in binders for thermally curable reactive multisubstance mixtures. In the

context of the present invention, thermally curable reactive multisubstance mixtures are coating compositions, adhesives or sealing compounds which in addition to the binder or binders comprise at least one crosslinking agent which with the binders on heating constructs a three-dimensional thermoset network.

Such crosslinking reactions are customary and known in the fields of the coating compositions, adhesives and sealing compounds and are described, for example, in the article by M. Ooka and H. Ozawa, "Recent developments in crosslinking technology for coating resins", in Progress in Organic Coatings, Volume 23, 325 to 338, 1994. Of the numerous known crosslinking reactions, preference is given to crosslinking reactions

- between hydroxyl groups and functional groups which are able to react with hydroxyl groups, and

- between epoxide groups and carboxyl groups.

Accordingly, the monomers used include those which carry reactive functional groups which are able to undergo crosslinking reactions with the crosslinking agents. Examples of suitable monomers of this kind are

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from 1 500 to 5 000.

The glass transition temperature of the polyacrylate resins is determined by the nature and amount of the monomers used. The selection of the monomers may be made by the skilled worker with the aid of the following formula, by means of which the glass transition temperatures of polyacrylate resins may be approximately calculated:

10

$$n = x$$

$$1/T_g = \sum W_n/T_{g_n}; \sum_n W = 1$$

$$n = 1$$

15 T_g = glass transition temperature of the polyacrylate resin

W_n = weight fraction of the nth monomer

T_{g_n} = glass transition temperature of the homopolymer of the nth monomer

20 x = number of different monomers

Measures to control the molecular weight (e.g. selection of corresponding polymerization initiators, use of chain transfer agents, etc.) are part of the art knowledge of the skilled worker and need not be elucidated further here.

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For the present invention it is important that the above-described monomers are (co)polymerized in at least one reactive diluent for thermally curable
5 reactive multisubstance mixtures.

In accordance with the invention, suitable reactive diluents as the reaction medium are all those which, during the known crosslinking reactions which take
10 place in the multisubstance mixtures of the invention, are incorporated into the binder and which do not hinder, let alone prevent, the homopolymerization or copolymerization of the monomers. The skilled worker will therefore be able to select the reactive diluents
15 that are suitable in each case with the aid of his or her general knowledge in the art, where appropriate with the assistance of simple preliminary tests.

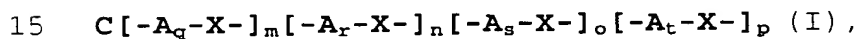
In accordance with the invention, advantageous reactive
20 diluents are those which participate in the crosslinking

- of hydroxyl-containing compounds which carry functional groups that are reactive toward
25 hydroxyl groups, or

- compounds containing epoxide groups with carboxyl-containing compounds.

Accordingly, the reactive diluents which are particularly preferred in accordance with the invention contain hydroxyl groups or epoxide groups.

Examples of reactive diluents particularly preferred in accordance with the invention are hyperbranched compounds containing a tetrafunctional central group derived from ditrimethylolpropane, diglycerol and/or ditrimethylolethane or a tetrafunctional central group of the general formula I



in which the indices and variables have the following definitions:

$m + n + o + p = 4$; where

m is an integer from 1 to 3, and

n , o and p are 0 or an integer from 1 to 3;

q , r , s and t are an integer from 1 to 5, where $q \geq r$,

s , t , especially $q > r$, s , t ;

X is $-O-$, $-S-$ or $-NH-$;

A is $-\text{CR}_2-$; where

R is -H, -F, -Cl, -Br, -CN, -NO₂, C₁-C₃ alkyl or haloalkyl or C₁-C₃ alkoxy radical or, if q, r, s and/or t are at least 2, R is a C₂-C₄ alkanediyl and/or oxaalkanediyl radical having 2 to 5 carbon atoms and/or an oxygen atom -O- which bridges from 3 to 5 carbon atoms of the radical -A-.

10

The term "derived" relates in this case to the imaginary abstraction of the hydrogen atoms from the hydroxyl groups of the tetraols.

15 In accordance with the invention, the central groups I
are of advantage and are therefore used with particular
preference.

In the general formula I the indices q, r, s and t denote integers from 1 to 5. In this case the index q may be equal to the indices r, s and t . In that case the resulting central groups I are symmetrical.

Examples of suitable symmetrical central groups I for
25 use in accordance with the invention are derived from
symmetrical tetraols such as pentaerythritol,
tetrakis(2-hydroxyethyl)methane or tetrakis-
(3-hydroxypropyl)methane.

In accordance with the invention, central groups I in which the index q is greater than the indices r, s and t and therefore has a value of at least 2 are of advantage and are therefore used with very particular
5 preference. In that case, the resulting central groups I are asymmetric.

In the general formula I the indices m, n, o and p then add up to 4. The index m is always greater than 0 and
10 represents an integer from 1 to 3, especially 1.

Subject to the above conditions, the indices n, o and p have the value 0 or represent an integer from 1 to 3. This means that it is not possible for each of these
15 indices to adopt the value 0.

In accordance with the invention, the following value combinations of the indices are of advantage:

- 20 m = 1 and n, o, p = 1;
m = 1, n = 2, o, p = 1;
m = 1, n = 2, o = 1 and p = 0;
m = 1, n = 3, o, p = 0;
- 25 m = 2, n = 1, o = 1 and p = 0;
m = 2, n = 2 and o, p = 0;
- m = 3, n = 1 and o, p = 0.

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Of these numerical combinations, those in which $m = 1$ are particularly advantageous.

In accordance with the invention, the following
5 numerical combinations of the indices are of advantage:

$q = 2, r, s$ and/or $t = 1$;

$q = 3, r, s$ and/or $t = 1$ and/or 2 ;

$q = 4, r, s$ and/or $t = 1, 2$ and/or 3 ;

10 $q = 5, r, s$ and/or $t = 1, 2, 3$ and/or 4 .

The variable $-X-$ in the general formula I denotes
divalent oxygen atoms $-O-$ or sulfur atoms $-S-$ or a
secondary amino group $-NH-$. In accordance with the
15 invention it is advantageous for $-X-$ to be $-O-$.

The variable $-A-$ in the formula I denotes a divalent
radical $-CR_2-$.

20 The radical R therein represents hydrogen atoms $-H$,
fluorine atoms $-F$, chlorine atoms $-Cl$, bromine atoms
 $-Br$, nitrile groups $-CN$, nitro groups $-NO_2$, or C_1-C_3
alkyl or haloalkyl or C_1-C_3 alkoxy groups. Examples of
suitable groups of this kind are methyl, ethyl, propyl,
25 trifluoromethyl, trichloromethyl, perfluoroethyl,
perfluoropropyl, methoxy, ethoxy or propoxy groups.

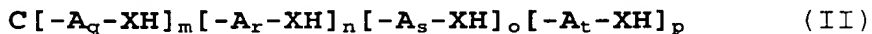
Of advantage in accordance with the invention are
hydrogen atoms or methyl groups, which are therefore

used with preference. In particular, hydrogen atoms are used. Accordingly, the variables -A- particularly preferred in accordance with the invention are methylene groups.

5

If in the general formula I at least one of the indices q, r, s and/or t represents at least the number 2, the radical R may also represent a C₂-C₄ alkanediyl and/or oxaalkanediyl radical which cyclically bridges from 2
10 to 5 carbon atoms of the radical -A-. Alternatively, the radical -R- may represent an oxygen atom -O- which cyclically bridges from 3 to 5 carbon atoms in the radical -A-. Formed in this way are cyclopentane-1,2- or 1,3-diyl groups, tetrahydrofuran-2,3-, -2,4-, -2,5-
15 or -3,4-diyl groups, cyclohexane-1,2-, -1,3- or -1,4-diyl groups or tetrahydropyran-2,3-, -2,4-, -2,5- or -2,6-diyl groups, but not epoxide groups.

Examples of central groups I which are especially
20 advantageous in accordance with the invention are derived from the following tetraols of the general formula II:



25

In the general formula II the indices and the variables have the same definitions as indicated above in connection with the general formula I. In accordance with the invention it is of particular advantage if the

variable X is an oxygen atom -O-.

Accordingly, for the preparation of the central group I and of the compounds to be used in accordance with the invention, the tetraols of the general formula II are of particular advantage and are therefore used with particular preference. In the text below they are referred to for brevity as "tetraols II".

10 Examples of very especially suitable tetraols II for use in accordance with the invention are the symmetrical tetraols pentaerythritol, tetrakis(2-hydroxyethyl)methane or tetrakis(3-hydroxypropyl)-methane or the asymmetric tetraols (II1) to (II10):

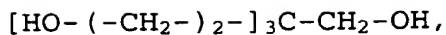
15
HO-(-CH₂-)₂-C(-CH₂-OH)₃,
(II1)

HO-(-CH₂-)₃-C(-CH₂-OH)₃,
20 (II2)

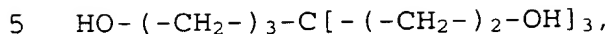
HO-(-CH₂-)₄-C(-CH₂-OH)₃,
(II3)

25 HO-(-CH₂-)₅-C(-CH₂-OH)₃,
(II4)

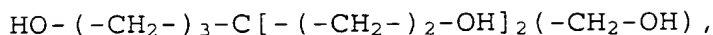
[HO-(-CH₂-)₂-]₂C(CH₂-OH)₂,
(II5)



(II6)

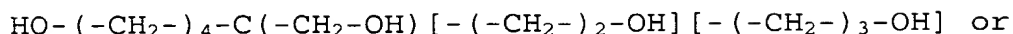


(II7)

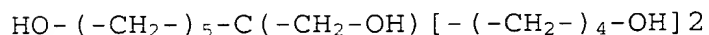


(II8)

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(II9)



15 (II10).

Of these, particular attention is drawn to the tetraol
(III1) (2,2-bishydroxymethyl-1,4-butanediol; homopenta-
erythritol) because it imparts especially advantageous
20 properties to the reactive diluents for use in
accordance with the invention and hence to the
compositions of the invention. For this reason it is
used with very particular preference.

25 In the reactive diluents whose use is particularly
preferred in accordance with the invention, the
variables -X- described above are connected by way of
spacer groups to in each case one hydroxyl group. This
also applies analogously to the central groups which

are derived from the tetraols ditrimethylolpropane,
diglycerol or ditrimethylolethane whose oxygen atoms
correspond to the variables -X-. The subsequent
description of the spacer groups therefore also applies
5 to these central groups which are different from the
central groups I.

In accordance with the invention, all divalent organic
radicals R^1 are suitable as spacer groups.

10

Examples of highly suitable divalent organic radicals
 R^1 are those derived from the following compounds:

(i) an alkane, alkene, cycloalkane, cycloalkene,
15 alkylcycloalkane, alkylcycloalkene, alkenylcyclo-
alkane, or alkenylcycloalkene, aromatic and
heteroaromatic and also an alkyl-, alkenyl-,
cycloalkyl-, cycloalkenyl-, alkylcycloalkyl-,
alkylcycloalkenyl-, alkenylcycloalkyl- or
20 alkenylcycloalkenyl-substituted aromatic or
heteroaromatic; or

(ii) an abovementioned radical which contains at least
one heteroatom in the chain and/or in the radical;
25 or

(iii) a radical specified under (i) or (ii) whose chain
and/or ring is substituted.

Examples of suitable substituents, for use in accordance with the invention, of the radicals R^1 are all organic radicals which are substantially inert, i.e., which do not undergo any reactions with the compounds used for the construction of the reactive diluents which are particularly preferred in accordance with the invention, or which are used for further reaction thereof, especially halogen atoms, nitro groups, nitrile groups or alkoxy groups.

10

The spacer groups are connected in particular by way of carbonyl groups to the central groups I or to the central groups which are derived from the other said tetraols.

15

Examples of organic compounds which are especially suitable for the preparation of these spacer groups are epsilon-caprolactone, hexahydrophthalic acid, hexahydrophthalic anhydride, phthalic acid, phthalic anhydride, hexahydroterephthalic acid, terephthalic acid, fumaric acid, maleic acid, maleic anhydride, itaconic acid, itaconic anhydride, oxalic acid, malonic acid, malonic anhydride, succinic acid, succinic anhydride, glutaric acid, glutaric anhydride, adipic acid, adipic anhydride, pimelic acid, suberic acid, azelaic acid, sebacic acid or decane-, undecane- or dodecanedicarboxylic acid. Of these, epsilon-caprolactone, maleic acid or maleic anhydride and hexahydrophthalic anhydride are especially suitable and

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are therefore used with particular preference.

In the preparation of the particularly preferred reactive diluents for use in accordance with the invention, the tetraols II or the other said tetraols are reacted with the abovementioned difunctional compounds to form an intermediate into which the hydroxyl groups may be introduced.

Suitable for this purpose are all organic compounds which are able to react with the intermediates to form a hydroxyl group or with retention of a hydroxyl group. In accordance with the invention it is of advantage to use a compound which reacts with the intermediates to form a hydroxyl group.

Examples of highly suitable organic compounds of this kind are compounds containing epoxide groups, especially compounds containing glycidyl groups.

Examples of highly suitable compounds containing epoxide groups, especially compounds containing glycidyl groups, are ethylene oxide, propylene oxide, epichlorohydrin, glycidol, glycidyl ether, especially aryl and alkyl glycidyl ethers, or glycidyl esters, especially the glycidyl esters of tertiary, highly branched, saturated monocarboxylic acids marketed under the trade name Versatic[®] acids by Deutsche Shell Chemie. Of these, the Versatic[®] acid glycidyl esters

are especially advantageous and are therefore used with very particular preference.

For the present invention it is important that the
5 above-described reactive diluents are liquid at room temperature. Consequently, either individual liquid hyperbranched compounds may be used, or liquid mixtures of these compounds. This is the case in particular when the high molecular weight and/or symmetry of the
10 hyperbranched compounds used means that, as individual compounds, they are solid. The skilled worker will therefore be able to select the appropriate hyperbranched compounds in a simple manner.

15 The reactive diluents which are particularly preferred may be prepared by the customary and known methods of preparing hyperbranched and dendrimeric compounds. Appropriate synthesis methods are described, for example, in the patents WO 93/17060 or WO 96/12754 or
20 in the book by G.R. Newkome, C.N. Moorefield and F. Vögtle, "Dendritic Molecules, Concepts, Syntheses, Perspectives", VCH, Weinheim, New York, 1996.

Further examples of reactive diluents particularly
25 preferred in accordance with the invention are the cyclic and/or acyclic C₉-C₁₆ alkanes functionalized with at least two hydroxyl groups or at least one hydroxyl group and at least one thiol group, and are referred to for brevity below as "functionalized alkanes".

The functionalized alkanes are derived from branched, cyclic or acyclic alkanes having from 9 to 16 carbon atoms, which in each case form the parent structure.

- 5 Examples of suitable such alkanes having 9 carbon atoms are 2-methyloctane, 4-methyloctane, 2,3-dimethylheptane, 3,4-dimethylheptane, 2,6-dimethylheptane, 3,5-dimethylheptane, 2-methyl-4-ethylhexane or isopropylcyclohexane.

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Examples of suitable such alkanes having 10 carbon atoms are 4-ethyloctane, 2,3,4,5-tetramethylhexane, 2,3-diethylhexane or 1-methyl-2-n-propylcyclohexane.

- 15 Examples of suitable such alkanes having 11 carbon atoms are 2,4,5,6-tetramethylheptane or 3-methyl-6-ethyloctane.

- 20 Examples of suitable such alkanes having 12 carbon atoms are 4-methyl-7-ethylnonane, 4,5-diethyloctane, 1'-ethylbutylcyclohexane, 3,5-diethyloctane or 2,4-diethyloctane.

- 25 Examples of suitable such alkanes having 13 carbon atoms are 3,4-dimethyl-5-ethylnonane or 4,6-dimethyl-5-ethylnonane.

An example of a suitable such alkane having 14 carbon atoms is 3,4-dimethyl-7-ethyldecane.

Examples of suitable such alkanes having 15 carbon atoms are 3,6-diethylundecane or 3,6-dimethyl-9-ethylundecane.

5 Examples of suitable such alkanes having 16 carbon
atoms are 3,7-diethyldodecane or 4-ethyl-6-
isopropylundecane.

Of these parent structures, the alkanes having 10 to 14
10 and especially 12 carbon atoms are particularly
advantageous and are therefore used with preference. Of
these, in turn, the octane derivatives are especially
advantageous.

15 For the present invention it is important that the functionalized alkanes which derive from these branched, cyclic or acyclic alkanes as parent structures are liquid at room temperature. Consequently, it is possible to use either individual
20 liquid functionalized alkanes or liquid mixtures of these compounds. This is the case in particular when the high number of carbon atoms in the alkane parent structure of the functionalized alkanes used means that, as individual compounds, they are solid. The
25 skilled worker will therefore be able to select the appropriate functionalized alkanes or reactive diluents in a simple manner.

For the invention it is also important that the

functionalized alkanes have a boiling point of more than 200, preferably 220 and in particular 240°C. Furthermore, they ought also to have a low evaporation rate.

5

In accordance with the invention it is of advantage, furthermore, if the functionalized alkanes are acyclic.

10 The functionalized alkanes have primary and/or secondary hydroxyl groups or primary and/or secondary hydroxyl groups and thiol groups. In accordance with the invention it is of advantage if primary and secondary groups of this kind are present in one functionalized alkane.

15

The functionalized alkanes are accordingly polyols or polyol-polythiols, but especially polyols. These compounds may be used individually or together as mixtures. Particular advantages result if the polyols
20 are diols and/or triols, but especially diols. They are therefore used with very particular preference.

Especially advantageous polyols are the positionally isomeric dialkyloctanediols, especially diethyloctane-
25 diols. Of these, particular attention is drawn to 2,4-diethyl-1,5-octanediol.

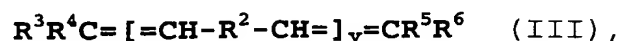
The reactive diluents described above are compounds which are known per se and can be prepared with the aid

of customary and known synthesis methods of organic chemistry, such as base-catalyzed aldol condensation, or are obtained as by-products of chemical industrial syntheses such as the preparation of 2-ethylhexanol.

5

Further examples of reactive diluents particularly preferred are obtained by subjecting oligomers of the formula III

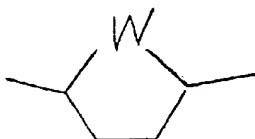
10



in which R^2 is $-(-CH_2-)_w-$,

in which the index w is an integer from 1 to 6, or

=



15

in which W is $-CH_2-$ or an oxygen atom;

R^3 , R^4 , R^5 and R^6 independently of one another are hydrogen atoms or alkyl; and

20

the index v is an integer from 1 to 15;

to hydroformylation and reducing the resultant products III, containing aldehyde groups, to the polyols III, which if desired are partially or fully hydrogenated.

25

The index v in the formula III represents the number of

divalent radicals R^2 introduced by ring-opening metathesis reaction into the oligomers I derived from cyclic olefins such as, for example, cyclopropene, cyclopentene, cyclobutene, cyclohexene, cycloheptene, norbornene, 7-oxanorbornene or cyclooctene. Preferably, as great as possible a fraction of the oligomer mixtures III useful according to the invention, such as, for example, at least 40% by weight (determined by the area integration of the gas chromatograms; instrument: Hewlett Packard; detector: flame ionization detector; column: DB 5.30 m x 0.32 mm, coverage 1 μ ; temperature program: 60°C 5 min., isothermal, heating rate 10°C/min, max.: 300°C), have a value of $v > 1$. The value v and thus the degree of ring-opening metathesis can be influenced, as specified later on below, by the activity of the metathesis catalyst that is used.

The radicals R^3 , R^4 , R^5 and R^6 are independently of one another hydrogen or alkyl, the expression "alkyl" embracing straight-chain and branched alkyl groups.

The alkyl groups in question are preferably straight-chain or branched C_1 - C_{15} , preferably C_1 - C_{10} , with particular preference C_1 - C_5 , alkyl groups. Examples of alkyl groups are, in particular, methyl, ethyl, propyl, 1-methylethyl, butyl, 1-methylpropyl, 2-methylpropyl, 1,1-dimethylethyl, n-pentyl, 1-methylbutyl, 2-methylbutyl, 3-methylbutyl, 1,2-dimethylpropyl, 1,1-dimethylpropyl, 2,2-dimethylpropyl, 1-ethylpropyl,

n-hexyl, 1-methylpentyl, 2-methylpentyl, 3-methyl-
pentyl, 4-methylpentyl, 1-2-dimethylbutyl,
1,3-dimethylbutyl, 2-3-dimethylbutyl, 1,1-dimethyl-
propyl, 1,2,2-trimethylpropyl, 1-ethylbutyl, 2-ethyl-
5 butyl, 1-ethyl-2-methylpropyl, n-heptyl, 1-methylhexyl,
1-ethylpentyl, 2-ethylpentyl, 1-propylbutyl, octyl,
decyl, dodecyl, etc.

The degree of branching and the number of carbon atoms
10 of the terminal alkyl radicals R^3 , R^4 , R^5 and R^6 depend
on the structure of the acyclic monoolefins of the
hydrocarbon mixture used and on the activity of the
catalyst. As detailed below, the catalyst activity
influences the degree of cross-metathesis (self-
15 metathesis) of the acyclic olefins, with formation of
structurally new olefins, into which then, formally,
cyclopentene is inserted in a ring-opening metathesis
polymerization.

20 Preference is given to the use of oligomer mixtures
containing an increased fraction of oligomers having
only one terminal double bond. The oligomer is
preferably prepared by reacting a hydrocarbon mixture
comprising a cyclic monoolefin such as cyclopropene,
25 cyclobutene, cyclopentene, cyclohexene, cycloheptene,
cyclooctene, norbornene or 7-oxanorbornene, and acyclic
monoolefins as well, obtained from the processing of
petroleum by cracking (C_5 cut), in a homogeneous or
heterogeneous metathesis reaction.

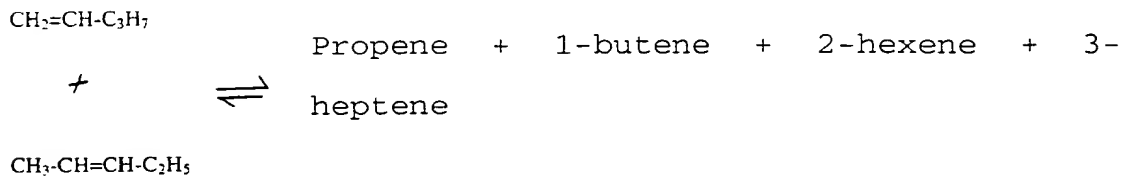
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The metathesis reaction formally comprises

- 5 a) the disproportionation of the acyclic monoolefins
of the hydrocarbon mixture by cross-metathesis,
- b) the oligomerization of the cyclic monoolefin by
ring-opening metathesis,
- 10 c) chain termination by reaction of the oligomers
from b) with an acyclic olefin of the hydrocarbon
mixture or of a product from a),
- it being possible to traverse steps a) and/or b) and/or
15 c) a number of times, individually or in combination.

Step a)

The cross-metathesis of the acyclic monoolefins will be
20 illustrated using the example of the metathesis of
1-pentene and 2-pentene:



A combination of cross-metathesis of different acyclic
25 olefins and self-metathesis of identical acyclic
olefins, such as, for example, the self-metathesis of

1-pentene to ethene and 4-octene, and multiple traversal of this reaction, produces a large number of monoolefins of different structure and with different carbon atom numbers, which form the end groups of the
5 oligomers I. The proportion of cross-metathesis products, which increases as the activity of the catalyst used goes up, also influences the double bond content of the oligomers. Thus, for example, in the case of the self-metathesis of 1-pentene, described
10 above, ethene is liberated, which may if appropriate escape in the form of a gas, removing one double bond equivalent from the reaction. At the same time, there is an increase in the fraction of oligomers without terminal double bonds. In the above example, therefore,
15 an oligomer without terminal double bonds is formed, for example, by insertion of cyclic monoolefin into 4-octene.

Step b)

20

The average number of insertions of the cyclic monoolefin into the growing chain in a ring-opening metathesis polymerization determines the average molecular weight of the resulting oligomer mixture I.
25 Preferably, oligomer mixtures I having an average molecular weight of at least 274 g per mole are formed by the process of the invention, which corresponds to an average number of three units of a cyclic monoolefin per oligomer.

Step c)

Chain termination takes place by reaction of oligomers that still have an active chain end in the form of a catalyst complex (alkylidene complex) with an acyclic olefin; in the course of this reaction, ideally, an active catalyst complex is recovered. In that case, the acyclic olefin may originate unchanged from the hydrocarbon mixture originally used for the reaction, or may have been modified beforehand in a cross-metathesis in accordance with stage a).

Very generally, the process is suitable for preparing oligomers III from hydrocarbon mixtures which comprise acyclic and cyclic monoolefins: monoolefins such as, for example, cyclobutene, cyclopentene, cyclohexene, cycloheptene, norbornene or 7-oxanorbornene, especially cyclopentene. Variants of this process are described, for example, in the article by M. Schuster and S. Bleckert in *Angewandte Chemie*, 1997, Volume 109, pages 2124 to 2144.

Preference is given to the use of a hydrocarbon mixture obtained industrially in the processing of petroleum, it being possible if desired to subject said mixture to catalytic partial hydrogenation beforehand in order to remove dienes. A particularly suitable mixture for use in the present process is, for example, a mixture enriched in saturated and unsaturated C₅ hydrocarbons

(C₅ cut). To obtain the C₅ cut it is possible, for example, first to subject pyrolysis benzine obtained in the steam cracking of naphtha to a selective hydrogenation in order to convert, selectively, the
5 dienes and acetylenes present into the corresponding alkanes and alkenes, and subsequently to subject the product to a fractional distillation, producing firstly the C₆-C₈ cut, which is important for further chemical syntheses and comprises the aromatic hydrocarbons, and
10 secondly the C₅ cut, which is used for the process of the invention.

The C₅ cut generally has a total olefin content of at least 30% by weight, preferably at least 40% by weight,
15 in particular at least 50% by weight.

Suitable in this context are C₅ hydrocarbon mixtures having a total cyclopentene content of at least 5% by weight, preferably at least 10% by weight, in
20 particular at least 12% by weight, and generally not more than 30% by weight, preferably not more than 20% by weight.

Furthermore, suitable C₅ hydrocarbon mixtures have a
25 proportion of pentene isomers among the acyclic monoolefins of at least 70% by weight, preferably at least 80% by weight, in particular at least 90% by weight.

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The preparation process can also be performed with a C₅ cut which is obtained industrially and has a total olefin content of, for example, from 50 to 60% by weight, such as about 56%, a cyclopentene content of, for example, from 10 to 20% by weight, such as about 15% by weight, and a pentene isomer content of, for example, from 33 to 43% by weight, such as about 38% by weight, with about 16% by weight being accounted for by the n-pentene and about 22% by weight by isomeric pentenes.

In one specific embodiment, the hydrocarbon mixture used in the preparation process comprises the C₅ cut and a petroleum fraction containing acyclic C₄ olefins (raffinate 2).

In another specific embodiment of the preparation process, a hydrocarbon mixture is used which comprises the C₅ cut and ethene. In this case, oligomer mixtures III having an increased double bond content are obtained. This is achieved first by ethenolysis of the acyclic n- and iso-pentenenes present in the C₅ cut to give shorter-chain α -olefins, such as propene and 1-butene, which react with cyclopentene in a ring-opening metathesis reaction to form oligomers III having in each case one terminal double bond. In addition, in the presence of ethene, the self-metathesis of the acyclic olefins to form further ethene, such as, for example, the self-metathesis of

1-pentene to form ethene and 4-octene, which as a chain terminating reagent leads to products without terminal double bonds, is suppressed. Secondly, a further increase in the double bond content is achieved by
5 ethenolysis of cyclopentene with ethene to give 1,6-heptadiene. This results in sequences of oligomers each of which have two terminal double bonds. When oligomer mixtures III obtained in this way, having an increased double bond content, are used for the
10 functionalization, the result is preferably oligomer mixtures III having an increased density of functionalities.

Suitable catalysts for the metathesis are known from
15 the prior art and include homogeneous and heterogeneous catalyst systems. In general, the catalysts suitable for the preparation process are based on a transition metal from transition group 6, 7 or 8 of the Periodic Table, with preference being given to the use of
20 catalysts based on Mo, W, Re and Ru.

Suitable homogeneous catalyst systems are generally transition metal compounds, which, if appropriate in combination with a cocatalyst and/or, if appropriate,
25 in the presence of the olefin reactants, are capable of forming a catalytically active metal carbene complex. Such systems are described, for example, by R.H. Grubbs in Comprehensive Organometallic Chemistry, Pergamon Press, Ltd., New York, Volume 8, page 499 ff. (1982).

Suitable catalyst/cocatalyst systems based on W, Mo and Re may comprise, for example, at least one soluble transition metal compound and an alkylating agent. Examples include MoCl_2 $(\text{NO})_2(\text{PR}_3)_2/\text{Al}_2(\text{CH}_3)_3\text{Cl}_3$; WCl_6/BuLi ; $\text{WCl}_6/\text{EtAlCl}_2(\text{Sn}(\text{CH}_3)_4)/\text{EtOH}$; $\text{WOCl}_4/\text{Sn}(\text{CH}_3)_4$; $\text{WOCl}_2(\text{O}-[2,6-\text{Br}_2-\text{C}_6\text{H}_3])/\text{Sn}(\text{CH}_3)_4$; $\text{CH}_3\text{ReO}_3/\text{C}_2\text{H}_5\text{AlCl}_2$, with the four last-mentioned ones being preferred for the process of the invention.

10 Further transition metal-alkylidene complexes suitable as metathesis catalysts are described by R.R. Schrock in Accounts of Chemical Research, Volume 23, page 158 ff. (1990). In general, the complexes in question are tetracoordinated Mo- and W-alkylidene complexes
15 additionally containing two bulky alkoxy ligands and one imido ligand. For the process of the invention, preference is given to $((\text{CH}_3)_3\text{CO})_2\text{Mo}(=\text{N}-[2,6-(i-\text{C}_3\text{H}_7)_2-\text{C}_6\text{H}_3])(=\text{CHC}(\text{CH}_3)_2\text{C}_6\text{H}_5)$ and $[(\text{CF}_3)_2\text{C}(\text{CH}_3)\text{O}]_2\text{Mo}(=\text{N}-[2,5-(i-\text{C}_3\text{H}_7)=\text{C}_6\text{H}_3])(=\text{CH}(\text{CH}_3)_2\text{C}_6\text{H}_5)$.

20

In particular, homogeneous metathesis catalysts used are the catalysts described in Angewandte Chemie, Volume 107, pages 2179 ff. (1995), in Journal of the American Chemical Society, Volume 118, page 100 ff. (1996), and in Journal of the Chemical Society, Chemical Communications, page 1127 ff. (1995). In particular, these include $\text{RuCl}_2(=\text{CHR})(\text{PR}'_3)_2$, preferably $\text{RuCl}_2(=\text{CHC}_6\text{H}_5)(\text{P}(\text{C}_6\text{H}_{11})_3)_2$, $(\eta^6\text{-p-cymene})\text{RuCl}_2(\text{p}(\text{C}_6\text{H}_{11})_3)$ and 3 molar equivalents of diazoalkane $((\text{CH}_3)_3\text{SiCHN}_2$ or

$C_6H_5CHN_2$) produced "in situ".

Suitable heterogeneous catalyst systems generally comprise a transition metal compound on an inert support, said compound being capable without a cocatalyst of forming a catalytically active alkylidene complex by reaction with the olefin reactants. It is preferred to use Re_2O_7 and CH_3ReO_3 .

Suitable inorganic supports are the oxides customary for this purpose, especially silicon oxides and aluminum oxides, aluminosilicates, zeolites, carbides, nitrides, etc., and mixtures thereof. Preferred supports used are Al_2O_3 , SiO_2 and mixtures thereof, in combination with B_2O_3 and Fe_2O_3 if desired.

The aforementioned homogeneous and heterogeneous catalyst systems differ greatly in their catalytic activity, so that the individual catalysts may have different optimum reaction conditions for the metathesis. As already described above, the catalytic activity with respect to the cross-metathesis (step a)) also influences the product distribution of the oligomer mixtures I derived from cyclopentene. For instance, the ruthenium-based homogeneous catalyst systems $RuCl_2(=CHC_6H_5)(P(C_6H_{11})_3)_3$, (η^6 -p-cymene) $RuCl_2(P(C_6H_{11})_3)$ / $(CH_3)_3SiCHN_2$ and (η^6 -p-cymene) $RuCl_2(P(C_6H_{11})_3)/C_6H_5CHN_2$ are particularly suitable for the preparation process. Of

these, the first-mentioned ruthenium complex has a higher catalytic activity than the two last-mentioned ones, which under otherwise identical reaction conditions leads to higher space/time yields. At the same time, however, there is also an increased incidence of cross-metathesis in the case of the first complex, with the release, in part, of ethene as well, with the consequence that the resulting oligomer mixture III derived from cyclopentene has a somewhat smaller fraction of double bonds, which is manifested, for example, in a lower iodine number. Furthermore, owing to the cross-metathesis, a larger number of acyclic olefins without terminal double bonds is available, so that using the first-mentioned homogeneous ruthenium catalyst the proportion of oligomers I derived from cyclopentene having only one, or no, terminal double bond is increased. The two last-mentioned ruthenium complexes have a somewhat lower catalytic activity than the first-mentioned one, so that using them, in accordance with the process of the invention, cyclopentene-derived oligomer mixtures I are obtained which have a higher double bond fraction and thus a higher iodine number and also a larger fraction of terminal double bonds.

25

The heterogeneous catalyst systems as well have the above-described activity differences with the corresponding influence on the metathesis products. If CH_3ReO_3 on Al_2O_3 is used as a heterogeneous catalyst for

the preparation process, it has a higher catalytic activity than the corresponding homogeneous catalyst system comprising $\text{CH}_3\text{ReO}_3/(\text{C}_2\text{H}_5)\text{AlCl}_2$.

5 As a heterogeneous catalyst it is advantageous to use Re_2O_7 on Al_2O_3 . This has an activity approximately comparable with that of $\text{RuCl}_2(=\text{CHC}_6\text{H}_5)(\text{P}(\text{C}_6\text{H}_{11})_3)_2$ and also similar product distribution, and may be used again following regeneration in a stream of air at
10 elevated temperatures, such as about 550°C , for example.

If desired, therefore, depending on the catalyst used, it is possible to obtain cyclopentene-derived oligomer
15 mixtures III having varying double bond fractions and varying fractions of terminal double bonds.

In one specific embodiment of the preparation process, the metathesis catalyst used is a homogeneous,
20 ruthenium-based catalyst selected from $\text{RuCl}_2(=\text{CHC}_6\text{H}_5)(\text{P}(\text{C}_6\text{H}_{11})_3)_2$, $(\eta^6\text{-p-cymene})\text{RuCl}_2(\text{P}(\text{C}_6\text{H}_{11})_3)/(\text{CH}_3)_3\text{SiCHN}_2$ and $(\eta^6\text{-p-cymene})\text{RuCl}_2(\text{P}(\text{C}_6\text{H}_{11})_3)/\text{C}_6\text{H}_5\text{CHN}_2$, which is added to the reaction mixture as a solution in an organic solvent. Examples of suitable solvents are
25 aromatic hydrocarbons, such as toluene and xylene, and also halogenated alkanes, such as CH_2Cl_2 , CHCl_3 , etc.

In the case of reactive catalyst systems, the reaction temperature is from -20 to 200°C , preferably from 0 to

100°C, in particular from 20 to 80°C.

The reaction may be conducted at an increased pressure up to 5 bar, preferably up to 2 bar, or, with particular preference, at ambient pressure.

According to another specific embodiment of the preparation process, the metathesis catalyst used is a heterogeneous catalyst based on rhenium, selected from
10 $\text{CH}_3\text{ReO}_3/\text{Al}_2\text{O}_3$ preferably $\text{Re}_2\text{O}_7/\text{Al}_2\text{O}_3$, which is added to the reaction mixture without addition of solvent.

In the case of these catalysts, which are somewhat less active than the aforementioned homogeneous catalyst
15 systems, the reaction temperature is from about 20 to 120°C, in particular from 40 to 80°C.

The reaction is preferably conducted at an increased pressure from 2 to 20 bar, preferably from 3 to 15 bar,
20 in particular from 4 to 12 bar.

In terms of process regime, the preparation process can be performed either continuously or batchwise. Suitable reaction apparatuses are known to the skilled worker
25 and are described, for example, in Ullmanns Enzyklopädie der technischen Chemie, Volume 1, page 743 ff. (1951). They include stirred vessels for the batchwise process, for example, and tube reactors for the continuous process, for example.

According to a suitable batchwise variant of the preparation process it is possible, for example, to react the C₅ cut over one of the homogeneous ruthenium catalysts described above as being preferred, which if
5 desired is generated "in situ" in the reactor vessel, in a metathesis reaction to give the cyclopentene-derived oligomer mixture I.

According to a further suitable continuous variant of
10 the preparation process, the C₅ cut may be reacted, for example, in a tube reactor over one of the heterogeneous rhodium catalysts described above as being preferred.

15 In accordance with both possible process variants, and depending on the catalyst used and on the other reaction parameters, especially the reaction temperature, space/time yields of at least 10 g l⁻¹ h⁻¹, preferably at least 15 g l⁻¹ h⁻¹, are achieved.
20 Depending on the activity of the catalyst, however, it is also possible to obtain substantially higher space/time yields of up to about 500 g l⁻¹ h⁻¹.

The reaction mixture is separated by customary methods.
25 These include, for example, fractional distillation, at atmospheric or reduced pressure, or separation at elevated temperatures and atmospheric pressure in a falling-film evaporator. Low-boiling fractions containing still-unreacted olefins may if desired be

recycled to the reaction apparatus. Advantageously, more extensive reaction of the olefins present in the C₅ cut to oligomers III is achieved in the course of the preparation process, so that the low boilers which
5 are separated off comprise a C₅ hydrocarbon mixture with predominantly saturated cyclic and acyclic compounds.

As described above, the number and position of the
10 double bonds in the oligomers III may be influenced by the reaction conditions, especially the catalyst that is used in each case. According to the process described, cyclopentene oligomers III are obtained, where the iodine number is at least 250 g I₂/100 g
15 oligomers I, preferably at least 300 g I₂/100 g oligomers I.

The average molecular weight of these oligomers III derived from cyclic monoolefins, especially cyclo-
20 pentene, is at least 274 g/mol, which corresponds to an average conversion of three cyclopentene units per oligomer III, with chain termination by an acyclic pentene (and not by a cross-metathesis product) being assumed in this case.

25

In order to prepare the reactive diluents for use in accordance with the invention, the oligomers III detailed above are subjected to customary and conventional hydroformylation. Here, in general, the

oligomers III are reacted with hydrogen and carbon monoxide in the presence of catalysts containing suitable transition metals under atmospheric pressure or under superatmospheric pressure at temperatures from 5 50 to 150°C to give products III containing aldehyde groups.

An example of a suitable transition metal is rhodium.

10 The resultant products III are isolated and are reduced in a customary and known manner to the reactive diluents for use in accordance with the invention. Reducing agents suitable for this purpose are all those with which aldehyde groups can be reduced to hydroxyl 15 groups. Examples of suitable reducing agents are borohydrides, such as sodium tetrahydroboranate, or hydrogen in the presence of hydrogenation catalysts.

Examples of suitable hydroformylation and reduction 20 processes are described in the European patent EP-A-0 502 839.

The reactive diluents particularly preferred in accordance with the invention may be subjected in a 25 customary and known manner to partial or complete hydrogenation. Suitable reducing agents for this purpose include those mentioned above.

The reactive diluents particularly preferred in

accordance with the invention have a hydroxyl number (OHN) of from 200 to 650, in particular from 250 to 450. Their number-average molecular weight M_n , determined with the aid of gel permeation chromatography using polystyrene as the internal standard, lies within the range from 400 to 1 000, in particular from 400 to 600. Their mass-average molecular weight M_w , determined with the aid of gel permeation chromatography and polystyrene as the internal standard, lies within the range from 600 to 2 000, in particular from 600 to 1 100. The polydispersity M_n/M_w is from 1.4 to 3, in particular from 1.7 to 1.9.

15 A particularly outstanding reactive diluent for use in accordance with the invention has an OHN of 350, an M_n of 561 and an M_w of 1 068.

Further examples of reactive diluents which are particularly preferred in accordance with the invention are the epoxides described below, which before or after the (co)polymerization, and especially before the (co)polymerization, are reacted with low molecular mass monocarboxylic and/or polycarboxylic acids to give polyols, which in turn are used as reactive diluents in the case of the crosslinking by way of the hydroxyl

groups.

Further examples of reactive diluents particularly preferred in accordance with the invention are
5 compounds containing epoxide groups, such as

- glycidyl ethers of polyols or polyphenols such as glycerol, diglycerol, glucitol, erythritol, pentaerythritol, dipentaerythritol, trimethylolpropane, trimethylolethane, ditrimethylolpropane, ditrimethylolethane, tetrakis(2-hydroxyethyl)ethane, tetrakis(3-hydroxypropyl)methane, the above-described tetraols III1 to III10, the above-described hyperbranched compounds, the above-described functionalized alkanes, the above-described oligomeric polyols prepared by metathesis, hydroformylation and hydrogenation, pyrocatechol, resorcinol, hydroquinone, pyrogallol, phloroglucinol, p-(hydroxyphenyl)-phloroglucinol, 5-(7-hydroxynaphth-1-yl)-pyrogallol, bisphenol F, bisphenol A or novolaks;
10
15
20
- low molecular mass epoxy resins or oligomers which contain monomer (A6) in copolymerized form;
25
- glycidyl esters of Versatic® acids;

- epoxy resin esters of saturated and unsaturated fatty acids (epoxidized oils); and
- 5 - epoxidized triglycerides of natural oils and esters.

Of the reactive diluents described in detail above, the diethyloctanediols, especially 2,4-diethyloctane-1,5-
10 diol, and the oligomeric polyols prepared by metathesis, hydroformylation and hydrogenation, deserve particular attention. In accordance with the invention, these are used with very particular preference as reactive diluents.

15

A certain fraction of the reactive diluents for use in accordance with the invention in a composition of the invention may be modified, following the (co)polymerization, with suitable olefinically
20 unsaturated compounds, so that the composition of the invention may be cured both thermally and by actinic light and/or electron beams. Examples of suitable compounds for such a modification are the above-described monomers (A2), (A5) or (A6).

25

The (co)polymerization of the invention in the reactive

diluents used in accordance with the invention has no special features in terms of its method and instead takes place with the methods of continuous or batchwise homopolymerization or copolymerization that are
5 customary and known in the plastics field, under atmospheric pressure or superatmospheric pressure in stirred vessels, autoclaves, tube reactors or Taylor reactors.

10 Examples of suitable (co)polymerization processes are described in the patents DE-A-197 09 465, DE-C-197 09 476, DE-A-28 48 906, DE-A-195 24 182, EP-A-0 554 783, WO 95/27742 or WO 82/02387.

15 In accordance with the invention, Taylor reactors are advantageous and are therefore used in preference for the process of the invention.

Taylor reactors, which serve to convert substances
20 under the conditions of Taylor flow, are known. They consist essentially of two coaxial concentric cylinders of which the outer is fixed while the inner rotates. The reaction space is the volume formed by the gap between the cylinders. Increasing angular velocity ω_i
25 of the inner cylinder is accompanied by a series of different flow patterns which are characterized by a dimensionless parameter, known as the Taylor number Ta .

As well as the angular velocity of the stirrer, the Taylor number is also dependent on the kinematic viscosity ν of the fluid in the gap and on the geometric parameters, the external radius of the inner
5 cylinder r_i , the internal radius of the outer cylinder r_o and the gap width d , the difference between the two radii, in accordance with the following formula:

$$Ta = \omega_i r_i d \nu^{-1} (d/r_i)^{1/2} \quad (I)$$

10

where $d = r_o - r_i$.

At low angular velocity, the laminar Couette flow, a simple shear flow, develops. If the rotary speed of the
15 inner cylinder is increased further, then, above a critical level, alternately contrarotating vortices (rotating in opposition) occur, with axes along the peripheral direction. These vortices, called Taylor vortices, are rotationally symmetric and have a
20 diameter which is approximately the same size as the gap width. Two adjacent vortices form a vortex pair or a vortex cell.

The basis of this behavior is the fact that, in the
25 course of rotation of the inner cylinder with the outer cylinder at rest, the fluid particles that are near to the inner cylinder are subject to a greater centrifugal force than those at a greater distance from the inner cylinder. This difference in the acting centrifugal

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forces displaces the fluid particles from the inner to the outer cylinder. The centrifugal force acts counter to the viscosity force, since for the motion of the fluid particles it is necessary to overcome the friction. If there is an increase in the rotary speed, there is also an increase in the centrifugal force. The Taylor vortices are formed when the centrifugal force exceeds the stabilizing viscosity force.

10 In the case of Taylor flow with a low axial flow, each vortex pair passes through the gap, with only a low level of mass transfer between adjacent vortex pairs. Mixing within such vortex pairs is very high, whereas axial mixing beyond the pair boundaries is very low. A vortex pair may therefore be regarded as a stirred tank in which there is thorough mixing. Consequently, the flow system behaves as an ideal flow tube in that the vortex pairs pass through the gap with constant residence time, like ideal stirred tanks.

20

Of advantage in accordance with the Taylor reactors having an external reactor wall located within which there is a concentrically or eccentrically disposed rotor, a reactor floor and a reactor lid, which together define the annular reactor volume, at least one means for metered addition of reactants, and a means for the discharge of product, where the reactor wall and/or the rotor are or is geometrically designed in such a way that the conditions for Taylor vortex

flow are met over substantially the entire reactor length in the reactor volume, i.e. in such a way that the annular gap broadens in the direction of flow traversal.

5

As (co)polymerization initiators it is preferred to use initiators which form free radicals. The nature and amount of initiator are normally chosen so that the supply of radicals is very largely constant at the

10

polymerization temperature during the feed phase. As examples of initiators which can be used are the following: dialkyl peroxides, e.g. di-tert-butyl peroxide and dicumyl peroxide, hydroperoxides, e.g. cumene hydroperoxide and tert-butyl hydroperoxide, peresters, e.g. tert-butyl perbenzoate, tert-butyl perpivalate, tert-butyl per-3,5,5,5-trimethylhexanoate and tert-butyl per-2-ethylhexanoate, or disazo compounds such as azobisisobutyronitrile.

15

20

Besides the reactive diluents for use in accordance with the invention, the reaction medium may also comprise further constituents in minor amounts. In the context of the present invention, the term "minor amount" means a fraction of other constituents which does not adversely affect, but which instead advantageously varies, the advantageous profile of properties of the reaction medium that is brought about

25

Patent 4690860

by the reactive diluents.

Examples of suitable further constituents are water, carbon dioxide, organic solvents or additives which are
5 customary and known in the field of coating compositions, adhesives and sealing compounds. Examples of suitable additives are described below.

The polymerization conditions (reaction temperature,
10 feed time of the monomer mixture and polymerization initiators, possible use of molecular weight regulators, e.g. mercaptans, thioglycolic esters, alpha-diphenylethene, compounds containing nitroxyl radical groups, or hydrogen chloride) are selected so
15 that in particular the polyacrylates prepared with particular preference in accordance with the invention and used have a number-average molecular weight as indicated above (determined by gel permeation chromatography using polystyrene as calibrating
20 substance). The acid number may be adjusted by the skilled worker by using appropriate amounts of component (A5). The same applies to the adjustment of the hydroxyl number and the epoxide number; they can be controlled by way of the amount of component (A4)
25 and/or (A6) used.

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The compositions of the invention prepared in accordance with the procedure of the invention have the particular advantage that they may be used directly to prepare the multisubstance mixtures of the invention.

5

For this purpose, minor amounts of further homopolymers or copolymers may be added to them. In the context of the present invention, the term "minor amounts" indicates that the fractions used should only be those which do not adversely alter, but instead advantageously vary or further improve, the advantageous profile of properties of the compositions of the invention that is brought about by the (co)polymers prepared by the procedure of the invention.

10

15

Examples of suitable homopolymers or copolymers which may be added to the compositions of the invention are (meth)acrylate diols, polyethers, polycarbonates, polylactones, acrylated polyesters, acrylated polyurethanes, polyurethanes, polyesters or polyacrylates prepared in other ways.

20

Suitable polyacrylates are sold, for example, under the brand name Joncryl®, such as, for instance, Joncryl® SCX 912 and 922.5.

25

FOR FURTHER INFORMATION

Suitable polyester resins and/or alkyd resins are described, for example, in Ullmanns Encyklopädie der technischen Chemie, third edition, volume 14, Urban & Schwarzenberg, Munich, Berlin 1963, pages 80 to 89 and
5 pages 99 to 105, or in the following books: Résines Alkydes-Polyester by J. Bourry, Dunod, Paris 1952, Alkyd Resins by C.R. Martens, Reinhold Publishing Corporation, New York 1961 and Alkyd Resin Technology
10 by T.C. Patton, Interscience Publishers 1962.

Examples of suitable polyurethane resins are the resins described in the patents EP-A-0 708 788, DE-A-44 01 544 and DE-A-195 34 361.

15 Furthermore, the compositions of the invention may be diluted with customary and known organic solvents or they may be dispersed or dissolved in water or in aqueous media.

20 Furthermore, for the purposes of preparing the multisubstance mixtures of the invention, further constituents customary in the prior art in the fields of coating compositions, adhesives and sealing
25 compounds are added to the compositions of the invention.

In this context it is also possible to design the multisubstance mixtures of the invention as single-component systems or else as multicomponent systems.

5 Such systems differ essentially in the nature of the crosslinking agent used. In both cases, suitable crosslinking agents include all those which react under curing conditions with the reactive groups of the binders, especially the hydroxyl groups or the epoxide
10 groups. The difference is that, in the case of the multicomponent systems, the appropriate crosslinking agent, owing to its high reactivity, has to be stored separately from the other constituents until shortly before it is used.

15 Examples of suitable crosslinking agents are amino resins, beta-hydroxyalkylamides, resins or compounds containing siloxane groups, resins or compounds containing anhydride groups, resins or compounds
20 containing carboxyl groups, blocked and unblocked polyisocyanates or alkoxycarbonylaminotriazines, but especially blocked polyisocyanates or tris(alkoxycarbonylamino)triazines.

25 In both one-component and multicomponent systems, blocked polyisocyanates, or a mixture of blocked

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polyisocyanates, may be employed.

The blocked polyisocyanates which may be employed are preferably designed such that they contain both
5 isocyanate groups blocked with a blocking agent (Z1) and isocyanate groups blocked with a blocking agent (Z2), the blocking agent (Z1) being a dialkyl malonate or a mixture of dialkyl malonates, the blocking agent (Z2) being a blocking agent containing active methylene
10 groups, an oxime or a mixture of these blocking agents, and being different from (Z1), and the equivalents ratio between the isocyanate groups blocked with (Z1) and the isocyanate groups blocked with (Z2) being between 1.0:1.0 and 9.0:1.0, preferably between 8.0:2.0
15 and 6.0:4.0, and with particular preference between 7.5:2.5 and 6.5:3.5.

Further suitable blocking agents include dimethylpyrazole and/or substituted triazoles.

20

A polyisocyanate or a mixture of polyisocyanates is reacted in conventional manner with a mixture of the blocking agents (Z1) and (Z2), the mixture of the blocking agents (Z1) and (Z2) comprising the blocking
25 agents (Z1) and (Z2) in a molar ratio of between 1.0:1.0 and 9.0:1.0, preferably between 8.0:2.0 and

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6.0:4.0, and with particular preference between 7.5:2.5 and 6.5:3.5.

The polyisocyanate or mixture of polyisocyanates may be
5 reacted with the mixture of blocking agents (Z1) and (Z2) to the extent that isocyanate groups are no longer detectable. In practice, this may necessitate the use of very large excesses of blocking agents and/or very long reaction times.

10

It has been found that multisubstance mixtures, especially coating compositions, adhesives and sealing compounds, having good properties are obtained even when at least 50, preferably at least 70 percent of the
15 isocyanate groups of the polyisocyanate or of the mixture of polyisocyanates are reacted with the mixture of the blocking agents (Z1) and (Z2) and the remaining isocyanate groups are reacted with a hydroxyl-containing compound or with a mixture of hydroxyl-
20 containing compounds. Hydroxyl-containing compounds used are preferably low molecular mass aliphatic or cycloaliphatic polyols, such as neopentyl glycol, dimethylolcyclohexane, ethylene glycol, diethylene glycol, propylene glycol, 2-methyl-2-propylpropane-1,3-
25 diol, 2-ethyl-2-butylpropane-1,3-diol, 2,2,4-trimethylpentane-1,5-diol and 2,2,5-trimethylhexane-

1,6-diol, or hydroxyl-containing homopolymers or copolymers.

A suitable blocked polyisocyanate is also obtainable by
5 mixing polyisocyanates blocked with the blocking agent
(Z1) or (Z2) in a ratio such as to give a mixture in
which the equivalents ratio between the isocyanate
groups blocked with (Z1) and the isocyanate groups
blocked with (Z2) is between 1.0:1.0 and 9.0:1.0,
10 preferably between 8.0:2.0 and 6.0:4.0, and with
particular preference between 7.5:2.5 and 6.5:3.5.

In principle, all of the polyisocyanates known as paint
polyisocyanates may be used to prepare the blocked
15 polyisocyanates. It is, however, preferred to use
polyisocyanates whose isocyanate groups are attached to
aliphatic or cycloaliphatic radicals. Examples of such
polyisocyanates are hexamethylene diisocyanate,
isophorone diisocyanate, trimethylhexamethylene
20 diisocyanate, dicyclohexylmethane diisocyanate,
1,3-bis(2-isocyanatoprop-2-yl)benzene (TMXDI) and 1,4-
and 1,3-bis(isocyanatomethyl)cycloalkanes such as 1,4-
and 1,3-bis(isocyanatomethyl)cyclohexane and also
adducts of these polyisocyanates with polyols,
25 especially low molecular mass polyols, such as
trimethylolpropane, for example, and polyisocyanates

that are derived from these polyisocyanates and contain isocyanurate groups and/or biuret groups.

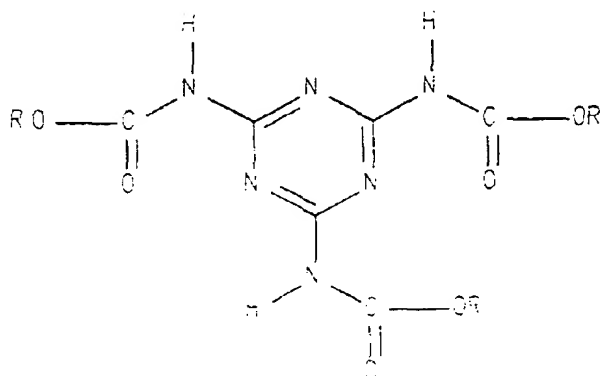
Polyisocyanates used with particular preference are
5 hexamethylene diisocyanate or isophorone diisocyanate,
polyisocyanates derived from these diisocyanates and
containing isocyanate, allophanate, uretdione,
iminooxadiazinedione, and/or biuret groups and
containing preferably more than two isocyanate groups
10 in the molecule, and reaction products of hexamethylene
diisocyanate and isophorone diisocyanate or of a
mixture of hexamethylene diisocyanate and isophorone
diisocyanate with 0.3-0.5 equivalent of a low molecular
mass polyol having a molecular weight of from 62 to
15 500, preferably from 104 to 204, in particular a triol,
such as trimethylolpropane, for example.

As blocking agents (Z1), dialkyl malonates or a mixture
of dialkyl malonates are used. Examples of dialkyl
20 malonates which can be used are dialkyl malonates
having 1 to 6 carbon atoms in each alkyl radical, such
as dimethyl malonate and diethyl malonate, preference
being given to the use of diethyl malonate. As blocking
agents (Z2), use is made of blocking agents containing
25 active methylene groups, oximes, and mixtures of these
blocking agents, all different from (Z1). Examples of

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blocking agents which may be used as blocking agents
(Z2) include the following: methyl, ethyl, propyl,
butyl, pentyl, hexyl, heptyl, octyl, nonyl, decyl or
dodecyl acetoacetate, acetone oxime, methyl ethyl
5 ketoxime, acetylacetone, formaldoxime, acetaldoxime,
benzophenoxime, acetoxime and diisobutyl ketoxime. As
blocking agent (Z2) it is preferred to use an alkyl
acetoacetate having from 1 to 6 carbon atoms in the
alkyl radical or a mixture of such acetoacetates or a
10 ketoxime or mixture of ketoximes. Particular preference
is given to the use of ethyl acetoacetate or methyl
ethyl ketoxime as blocking agent (Z2).

As crosslinkers it is also possible to use tris(alkoxy-
15 carbonylamino)triazines of the formula IV



(IV)

Examples of suitable tris(alkoxycarbonylamino)triazines
are described in the patents US-A-4,939,213,
US-A-5,084,541 and EP-A-0 624 577. Use is made in
20 particular of tris(methoxy-, tris(butoxy- and/or

tris(2-ethylhexoxycarbonylamino)triazines.

The methyl butyl mixed esters, the butyl 2-ethylhexyl mixed esters, and the butyl esters are of advantage.

- 5 They have the advantage over the straight methyl ester of better solubility in polymer melts, and also have less of a tendency to crystallize out.

It is likewise possible to use amino resins, examples
10 being melamine resins. In this context it is possible to use any amino resin suitable for transparent topcoats or clearcoats, or a mixture of such amino resins. Particularly suitable are the customary and known amino resins some of whose methanol and/or
15 methoxymethyl groups have been defunctionalized by means of carbamate or allophanate groups. Crosslinking agents of this kind are described in the patents US-A-4 710 542 and EP-B-0 245 700 and also in the article by B. Sing and coworkers, "Carbamylmethylated
20 Melamines, Novel Crosslinkers for the Coatings Industry" in Advanced Organic Coatings Science and Technology Series, 1991, Volume 13, pages 193 to 207.

Examples of suitable beta-hydroxyalkylamides are
25 N,N,N',N'-tetrakis(2-hydroxyethyl)adipamide or N,N,N',N'-tetrakis(2-hydroxypropyl)adipamide.

In the case of the multicomponent systems, especially the two-component systems, the crosslinking agent used comprises at least one unblocked polyisocyanate dissolved, if appropriate, in one or more organic solvents. In addition, however, it is also possible to use one of the above-described blocked polyisocyanates as well.

10 The unblocked or part-blocked polyisocyanates comprise any desired organic polyisocyanates, especially paint polyisocyanates, having free isocyanate groups attached to aliphatic, cycloaliphatic, araliphatic and/or aromatic moieties. Preference is given to using
15 polyisocyanates having from 2 to 5 isocyanate groups per molecule and having viscosities from 100 to 2 000 mPa.s (at 23 degrees C). It is also possible to use part-blocked polyisocyanates of the German patent DE-A-196 09 617. If desired, small amounts of organic
20 solvent may be added to the polyisocyanates, preferably from 1 to 25% by weight based on polyisocyanate alone, in order to improve the ease of incorporation of the polyisocyanate and, where appropriate, to lower the viscosity of the polyisocyanate to a level within the
25 abovementioned ranges.

Examples of suitable solvents for the polyisocyanates are ethoxyethyl propionate, butyl acetate and the like. Examples of suitable isocyanates are described in "Methoden der organischen Chemie", Houben-Weyl, Volume 14/2, 4th Edition, Georg Thieme Verlag, Stuttgart, 1963, pages 61 to 70, and by W. Siefken, Liebigs Annalen der Chemie, Volume 562, pages 75 to 136.

Further examples of suitable polyisocyanates are isocyanato-containing polyurethane prepolymers, which are prepared by reacting polyols with an excess of polyisocyanates and are preferably of low viscosity. It is also possible to use polyisocyanates containing isocyanurate, uretdione, iminooxadiazinedione, biuret, allophanate, urethane and/or urea groups. Polyisocyanates containing urethane groups, for example, are obtained by reacting some of the isocyanate groups with polyols, such as trimethylolpropane and glycerol, for example. Preference is given to using aliphatic or cycloaliphatic polyisocyanates, especially hexamethylene diisocyanate, dimerized and trimerized hexamethylene diisocyanate, isophorone diisocyanate, 2-isocyanatopropylcyclohexyl isocyanate, dicyclohexylmethane 2,4'-diisocyanate or dicyclohexylmethane 4,4'-diisocyanate, or mixtures of these polyisocyanates.

Very particular preference is given to using mixtures of polyisocyanates based on hexamethylene diisocyanate and containing uretdione and/or isocyanurate groups and/or allophanate groups, as are formed by catalytic
5 oligomerization of hexamethylene diisocyanate using appropriate catalysts. The polyisocyanate constituent may, furthermore, consist of any desired mixtures of the free polyisocyanates exemplified.

10 The multisubstance mixtures according to the invention may furthermore comprise UV absorbers; free-radical scavengers; crosslinking catalysts, especially organometallic compounds, preferably organotin/organo-
bismuth compounds or tertiary amines; rheology aids,
15 especially those known from the patents WO 94/22968, EP-A-0 276 501, EP-A-0 249 201 and WO 97/12945; pigments and fillers of any kind, examples being color pigments such as azo pigments, phthalocyanine pigments, carbonyl pigments, dioxazine pigments, titanium
20 dioxide, carbon black, iron oxides or chromium oxides and/or cobalt oxides, effect pigments such as metal flake pigments, especially aluminum flake pigments, and pearlescent pigments, or fillers such as chalk, calcium sulfates, barium sulfate, silicates such as talc or
25 kaolin, silicas, oxides such as aluminum hydroxide or magnesium hydroxide, or organic fillers such as textile

fibers, cellulose fibers, polyethylene fibers or wood
flour; slip additives; polymerization inhibitors;
defoamers; leveling agents or film formation
auxiliaries, e.g., cellulose derivatives; or other
5 additives, commonly employed in coating compositions,
adhesives or sealing compounds.

These additives are commonly used in an amount of up to
15% by weight, preferably from 2 to 9% by weight, based
10 on the weight of the respective multisubstance mixture
of the invention without pigments and without fillers.

The preparation of the multisubstance mixtures of the
invention has no special features in terms of the
15 technical process; rather, the customary methods, such
as the combining of the individual constituents and
their mixing with stirring, are employed. The
preparation of the multisubstance mixtures of the
invention consisting of two or more components is
20 likewise carried out by means of stirring or dispersion
using the commonly employed apparatuses, for example,
by means of dissolvers or by means of customary two-
component or multicomponent metering and mixing units.
The individual components are stored separately until
25 being used as intended.

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The multisubstance mixtures of the invention are used in particular as coating compositions, adhesives and sealing compounds.

5 The coating composition of the invention is used in particular to produce films, coated moldings, composites or complex components, especially vehicle bodies, which consist of or comprise films, glass, wood, paper and/or metal, by applying the coating compositions to the moldings, composites or complexed components in question and curing the resultant coating.

The coating composition of the invention is used preferably to produce single-coat or multicoat systems and with particular preference to produce topcoats. However, it may also be intended for the production of a clearcoat to be applied over a basecoat film, for example, a clearcoat of a multicoat system produced by the wet-on-wet technique. Furthermore, it may also be used as a primer, primer-surfacer, or as underbody protection. Of course, the plastics or the other substrates may also be coated directly with the clearcoat or topcoat material.

25

The coating compositions of the invention may be used

both for the OEM finishing and for the refinishing of vehicle bodies, especially automobile bodies, including mounted plastic components.

15 The application of the coating composition of the
invention and of the adhesive of the invention is
generally made using customary methods, such as
spraying, knife coating, dipping, brushing or coil
20 coating, for example.

introduced into the joints, by spraying or pouring, for example, and is thermally cured together, if desired, with the adhesives and/or coating compositions that are likewise used.

5

The coating compositions, adhesives or sealing compounds of the invention are preferably cured at temperatures from room temperature up to 240°C. Temperatures between 60 and 180°C are particularly preferred. In specific embodiments of the coating compositions of the invention it is also possible to employ lower curing temperatures of from 60 to 160°C.

Moldings, composites and complex components which consist of or comprise films, plastics, glass, wood, paper and/or metal and include at least one coat of the fully cured binder, at least one film of the fully cured adhesive and/or at least one joint sealed with a fully cured sealing compound of the invention have distinct advantages over conventional moldings, composites and components in terms of thermal stability, light stability, scratch resistance and weather stability, resulting over all in a longer lifetime.

25

Examples

Examp1 1

5 Preparation of a composition of the invention

A 4 l steel reactor suitable for the polymerization and equipped with reflux condenser and two metering vessels was charged with 935 g of 2,4-diethyloctane-1,5-diol and this initial charge was heated to 165°C. A mixture of 225 g of butyl acrylate, 225 g of styrene and 258 g of hydroxyethyl methacrylate and also 57 g of di-tert-butyl peroxide was added to this initial charge at a uniform rate over the course of three hours. Thereafter, the batch was stirred at 165°C for three hours. This gave a composition of the invention having a viscosity of 155.2 dPas. The composition of the invention was outstandingly suitable for the preparation of coating compositions, sealing compounds and adhesives.

Example 2

Preparation of a composition of the invention

25

In the steel reactor described above, 586.3 g of 2,4-

diethyloctane-1,5-diol were heated to 150°C. A mixture of 390.6 g of styrene, 254.6 g of methyl methacrylate, 339.4 g of tert-butylcyclohexyl acrylate, 101.8 g of butyl methacrylate and 611 g of hydroxypropyl methacrylate was added to this initial charge over the course of four hours. Starting 15 minutes before this feed, a mixture of 170.7 g of xylene and 41.1 g of di-tert-butyl peroxide was metered in over the course of four hours and 45 minutes. Thereafter, polymerization was continued for two hours and the resulting composition of the invention was diluted with 155.3 g of butyl acetate. The dilute composition of the invention had a viscosity of 1.3 dPas and was outstandingly suitable for preparing coating compositions.

Example 3

Preparation of a composition of the invention

The steel reactor described above was charged with 597 g of a hydroformylated and subsequently hydrogenated oligomer (oligomeric polyol) as hydroxyl-containing reactive diluent, and this initial charge was heated to 130°C.

The hydroformylated and hydrogenated oligomer itself had been prepared by metathesis of acyclic monoolefins and cyclic monoolefins, hydroformylation of the resulting oligomers and subsequent hydrogenation, the
5 cyclic monoolefin used being cyclopentene and acyclic monoolefins used being hydrocarbon mixtures obtained in petroleum processing by cracking (C_5 cut). The resultant oligomeric polyol had an OH number of 350, a viscosity of 27.2 dPas at 23° [cone and plate
10 viscometer], a number-average molecular weight M_n of 561 and a mass-average molecular weight M_w of 1 068.

A mixture of 120 g of styrene, 115.6 g of methyl methacrylate, 63.8 g of Methacrylester 13 (13-MA from
15 Röhm), 144 g of butyl methacrylate and 136.4 g of hydroxyethyl methacrylate was metered in to this initial charge over the course of four hours (monomer feed I). Commencing five minutes before this feed, a mixture of 90.4 g of the above-described oligomeric
20 polyol and 55.4 g of tert-butylperoxy-2-ethylhexanoate was metered in over the course of four hours and 30 minutes. After two hours and 30 minutes of the monomer feed I, a mixture of 57.2 g of hydroxyethyl acrylate, 27.5 g of acrylic acid and 19.7 g of the
25 above-described oligomeric polyol was metered in (monomer feed II). The reaction mixture was

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The resultant composition of the invention was
outstandingly suitable for the preparation of coating
5 compositions and sealing compounds.